GIAN Course on Rarefied & Microscale Gases and Viscoelastic Fluids: a Unified Framework

Lecture 2 Introduction to (Physical & Mathematical) Fluid Dynamics and CFD

Feb. 23rd ~ March 2nd, 2017

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I. Fluid dynamics: Eulerian vs. Lagrangian

- Eulerian description of the fluid motion: Properties are function of space and time Imaginary volume of a properly selected shape, fixed in space V.ndS represents in and out through the control surface
- Lagrangian approach: properties that are moving with the fluid (suitable for moving boundary problems)
- Conservation (neither be created nor destroyed): The sum of the time rate of mass within the region and the net flux of mass through a closed surface is zero



I. Fluid dynamics: conservation laws

 Conservation laws for mass, momentum and energy, in conjunction with the 2nd law of thermodynamics and the equation of state (EOS)

$$\frac{\partial}{\partial t} \int_{R} \begin{bmatrix} \rho \\ \rho \mathbf{u} \\ \rho E \end{bmatrix} dV + \oint_{S} \begin{bmatrix} \rho \mathbf{u} \\ \rho \mathbf{u} + p \mathbf{I} + \mathbf{\Pi} \\ (\rho E + p) \mathbf{u} + (\mathbf{\Pi} \cdot \mathbf{u} + \mathbf{Q}) \end{bmatrix} \cdot \mathbf{n} dS = 0,$$
$$p = \rho RT$$

where Π is viscous shear stresses (tensor) and

Q is heat flux (vector)

No approximations introduced so far!

I. Fluid dynamics: dimensionless numbers

 Dimensionless parameters (measuring relative importance of terms) in the stationary momentum equation

Viscous force (V) Inertial (I), Pressure (P)

Basis for model reduction and scaling laws

Reynolds no. Re
$$= \frac{I}{V} = \frac{\rho V^2}{\eta V/L} = \frac{\rho VL}{\eta}$$

Mach no. M² $= \frac{I}{P} = \frac{\rho V^2}{p} = \left(\frac{V}{\sqrt{RT}}\right)^2$

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I. Fluid dynamics: integral and differential forms

- Governing equations in integral and differential forms
 - Defined for volume and enclosed surface

$$\frac{\partial}{\partial t} \int_{R} \mathbf{U} dV + \oint_{S} \mathbf{F} \cdot \mathbf{n} dS = 0$$

$$\oint_{S} \mathbf{F} \cdot \mathbf{n} dS = \int_{R} \nabla \cdot \mathbf{F} dV; \text{ Gauss' theorem}$$

$$\frac{\partial \mathbf{U}}{\partial t} + \nabla \cdot \mathbf{F} = 0$$

• Defined for infinitesimal element

II. Navier-Stokes-Fourier

$$\frac{\partial}{\partial t} \begin{bmatrix} \rho \\ \rho \mathbf{u} \\ \rho E \end{bmatrix} + \nabla \cdot \begin{bmatrix} \rho \mathbf{u} \\ \rho \mathbf{u} + \frac{1}{\gamma M^2} p \mathbf{I} \\ \left(\rho E + \frac{1}{\gamma M^2} p \right) \mathbf{u} \end{bmatrix} + \frac{1}{\text{Re}} \nabla \cdot \begin{bmatrix} 0 \\ \mathbf{\Pi} \\ \mathbf{\Pi} \cdot \mathbf{u} + \frac{1}{Ec \operatorname{Pr}} \mathbf{Q} \end{bmatrix} = 0$$

Non-conserved variables
$$\mathbf{\Pi} = -2\eta \left[\nabla \mathbf{u} \right]^{(2)}, \mathbf{Q} = -k \nabla T$$

$$\Rightarrow \mathbf{U}(t, x, y, z) \text{ or } \rho(t, x, y, z), \mathbf{u}(t, x, y, z), p(t, x, y, z)$$

$$\Rightarrow \text{Drag} = x \text{ component of } \oint_{S} p_{w} \mathbf{n} dS + \oint_{S} \Pi_{w} \mathbf{n} dS + \oint_{S} \Pi_{w} \mathbf{s} dS$$

$$\Rightarrow C_{D} \equiv F_{D} / (0.5 \rho V^{2}S) = fn(\text{Re}, M)$$

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II. Navier-Stokes-Fourier

Navier (1822)

$$\Pi = -2\eta [\nabla u]^{(2)}$$

 Fourier (1822)
 $Q = -k\nabla T$

$$\begin{bmatrix} \Pi_{xx} & \Pi_{xy} \\ \Pi_{yx} & \Pi_{yy} \end{bmatrix} \leftarrow -2\eta(T) \begin{bmatrix} u_x - (u_x + v_y)/3 & (u_y + v_x)/2 \\ (v_x + u_y)/2 & v_y - (u_x + v_y)/3 \end{bmatrix}$$

with $\Pi_{xx} + \Pi_{yy} + \Pi_{zz} = 0$

 $u_x (\equiv \partial u / \partial x)$ case (compression and expansion)

$$u_y (\equiv \partial u / \partial y)$$
 case (velocity shear only)

$$-2\eta(T) \begin{bmatrix} 2u_x / 3 & 0 \\ 0 & -u_x / 3 \end{bmatrix}$$

Not like $(u_x)^2$

Newtonian or linear $-2\eta(T)\begin{bmatrix} 0 & u_y/2\\ u_y/2 & 0 \end{bmatrix}$ Uncoupled

Always vanishing normal stress Π_{xx} or Π_{yy}

$$\begin{bmatrix} Q_x \\ Q_y \end{bmatrix} \leftarrow -k(T) \begin{bmatrix} T_x \\ T_y \end{bmatrix}. \text{ Not like } (T_x)^2$$

III. Key issues: RMG vs turbulence

(Low Reynolds mesoscopic) fluid dynamics (RMG) is difficult because:



It involves **microscopic** collisional interactions among fluid particles and their **interplay** with the kinematic motion of particles in the macroscopic framework. This challenge is vividly illustrated by the high Mach number shock singularity problem (HMNP). (R. S. Myong PoF 2014)

(High Reynolds) fluid dynamics is difficult because:



At extremely small scales, even turbulent flow is very simple. It is smooth and well behaved. At larger scales, however, a fluid is subject to very few constraints. It can develop arbitrary levels of complexity like the effect of turbulence on separation. (P. L. Roe, "Future developments in CFD," ICAAT-GNU, May 2014)

III. Key issues: compressible vs incompressible

A common (but fatal when abused) logic

• Flow speed in typical micro- and nano-devices is low; that is, small *M*. Thus incompressible assumption and associated simplification like constant viscosity and thermal conductivity are well-justified.

Correct logic (Panton, *Incompressible Flow*, 2013, p. 248)

 When the temperature changes in the flow is finite, the flow must be considered; 1) (original) compressible, and 2) involving with the temperature dependence of transport coefficients, since

$$\eta / \eta_0 = 1 + \frac{d(\eta / \eta_0)}{d(T / T_0)} \left(\frac{T_w - T_0}{T_0}\right) \hat{T} + \cdots$$

IV. Introduction to CFD

CFD (Computational Fluid Dynamics)

A branch of fluid mechanics that uses numerical methods and algorithms to solve and analyze problems that involve fluid flows

Computational physics vs numerical analysis

The computational physics, which concerns the study of computational models for a given physical problem, as opposed to the analysis of numerical methods for a given computational model, becomes a key issue during the initial phase of the study of CFD algorithms for RMG.

$$x^{2} + 2x = 3$$
 vs $x^{2} + 2x = 3$
 $x^{2} + 2x + 1 - 1 = 3$ $x^{2} + 2x - 3 = 0$
 $(x+1)^{2} = 3 + 1 = 4$ $(x-1)(x+3) = 0$
 $x = -1 \pm 2 = 1, -3$ $x = 1, -3$

IV. CFD process

- Computational model & domain:
 - Boltzmann, Navier-Stokes-Fourier, etc.
- Geometry modeling
- Grid generation
- Flow solution
- Post-processing:
 - Contours, C_L , C_D , etc.
- Verification & validation

Memo

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IV. Overall CFD solution procedure



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Truncation error: Expanding the solution using Taylor series

$$u_{i}^{n+1} = u_{i}^{n} + \Delta t \left(\frac{\partial u}{\partial t}\right)_{i}^{n} + \frac{(\Delta t)^{2}}{2} \left(\frac{\partial^{2} u}{\partial t^{2}}\right)_{i}^{n} + \cdots, \quad u_{i-1}^{n} = u_{i}^{n} - \Delta x \left(\frac{\partial u}{\partial x}\right)_{i}^{n} + \frac{(\Delta x)^{2}}{2} \left(\frac{\partial^{2} u}{\partial x^{2}}\right)_{i}^{n} + \cdots$$

$$\frac{u_{i}^{n+1} - u_{i}^{n}}{\Delta t} + a \frac{u_{i}^{n} - u_{i-1}^{n}}{\Delta x} = 0 \implies \left(\frac{\partial u}{\partial t} + a \frac{\partial u}{\partial x}\right)_{i}^{n} = -\frac{\Delta t}{2} \left(\frac{\partial^{2} u}{\partial t^{2}}\right)_{i}^{n} + \frac{a \Delta x}{2} \left(\frac{\partial^{2} u}{\partial x^{2}}\right)_{i}^{n} + \cdots = O(\Delta t, \Delta x)$$

Consistent if the truncation error vanishes as the mesh is refined

 Stability: Errors (i.e. truncation, B.C.-related, round-off) do not grow as the calculation proceeds

$$u_{i}^{n} = e^{at} e^{j\frac{m\pi}{L}x} \Rightarrow \frac{u_{i}^{n+1} - u_{i}^{n}}{\Delta t} + a \frac{u_{i}^{n} - u_{i-1}^{n}}{\Delta x} = 0$$

$$\Rightarrow e^{a\Delta t} = f\left(\frac{a\Delta t}{\Delta x}, \frac{m\pi}{L}\Delta x\right); m \text{ no. of } \Delta x \text{ units; } L \text{ length}$$

- The stability requirement is that the amplification factor $|e^{a\Delta t}| \le 1$
- Courant-Friedrichs-Lewy (CFL) condition on time step and mesh spacing

$$\left|e^{a\Delta t}\right| \leq 1 \implies \frac{a\Delta t}{\Delta x} \leq 1$$

- A consistent stable numerical scheme is convergent (Lax's Equivalence Theorem)
- Convergence means that the numerical solution approaches the true solution of the PDEs as the mesh is refined



Truncation error:

- Usually 2nd-order accurate in space (and time)
 - Higher for wave propagation problems
- Lower than 2nd-order accurate in practice (degradation by B.C.)
- Grid refinement (convergence) study for error estimation:
 - Numerical solutions on a series of grids (coarse, reference, fine) with different cell sizes

Order of accuracy =

$$\ln\left[\left(\operatorname{Soln}_{\operatorname{coarse}} - \operatorname{Soln}\right) / \left(\operatorname{Soln} - \operatorname{Soln}_{\operatorname{fine}}\right)\right]$$

ln(refinement ratio)

V. Finite volume method

Discretization (explicit in time) of conservation laws in integral form

V. Finite volume method







Define a piecewise constant approximation of the solution at time n∆t Obtain the solution for the local Riemann problem at the cell interfaces Average the variables after a time interval ∆t and repeat until convergence of residuals

V. Boundary Conditions

- Thinking fluid dynamics first (before CFD) is essential
- Types of boundary conditions
 - Solid wall: no slip, no penetration, wall roughness for turbulence, temperature or heat flux specified
 - Far-field in external flows: in or out, supersonic or subsonic
 - Inflow and outflow in internal flows: velocity or pressure specified
 - Flow symmetry; boundary between blocks; periodic boundary
- An example: As the CFD solution converges, the velocity adjust itself such that the prescribed pressure B.C. is satisfied



Pressure inlet; P_{in} specified

Pressure outlet; P_{out} specified

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VI. Verification and validation (V & V)

- Verification: The process of determining that a model implementation accurately represents the developer's conceptual description of the model and the solution to the model.
- Validation: The process of determining the degree to which a model is an accurate representation of the real world from the perspective of the intended uses of the model



Oberkampf WL, Roy CJ. Verification and Validation in Scientific Computing. Cambridge University Press, 2010.

VI. Verification and validation (V & V)

Verification & validation: role of analytic solutions and benchmark cases



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VI. Validation process (sources of uncertainty)

- Sources of uncertainty in computational model:
 - Physical models: inviscid, viscous, incompressible
 - Auxiliary physical models: EOS, transport properties, turbulence model
 - Boundary conditions: Roughness, far-field, geometry representation
 - Initial conditions
 - Discretization, round-off, user errors
- Ingredients for validation of computational model:
 - Experimental data
 - Experimental uncertainty propagation
 - Computational model uncertainty propagation
 - Comparison error

VII. Tips in CFD practice

- "It is a poor workman who blames his tools the good man gets on with the job, given what he's got, and gets the best answer he can" (R.W. Hamming, You and Your Research)
- Solve the simple problems first (physics and grids)
- Study the benchmark problems
- Think FD before CFD (it's a bunch of numbers until FD comes in)
- Do not trust perfect agreement too much (often qualitative aspects more useful)

VII. Some words on CFD

- Garbage in, garbage out: the results are only as good as the input data.
- Skilled CFD practitioners cleverly use CFD to predict trends, rather than to guarantee absolute values.
- No one believes the CFD results except the one who performed the calculation, and everyone believes the experimental results except the one who performed the experiment.
- Navier-Stokes vs lattice Boltzmann: will it change the landscape of CFD
 "It may create some turbulence in the CFD market..."

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